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(54) Title: PROCESS FOR THE POLYMERIZATION OF α -OLEFINS, A CATALYST USED IN THE POLYMERIZATION AND ITS PREPARATION (57) Abstract In the polymerization of C ₃ -C ₁₂ - α -olefins, the activity of the catalyst and the isotacticity and molecular weight of the polymer product can be adjusted and improved in a controlled manner by a new process wherein: A) a catalyst system is prepared by bringing a support which comprises magnesium chloride, a derivative thereof or a reagent forming it into contact with at least titanium tetrachloride or a reagent forming it, in order to produce a titanated support; by bringing the titanated support into contact with at least a group 1, 2 or 13 metal compound which contains a C ₁ -C ₁₀ -alkyl and activates titanium tetrachloride to a catalytically active titanium group, in order to produce an activated support; and by bringing a substance selected from among the said support, titanated support and activated support into contact with at least one donor or a reagent forming it, in order to produce a catalyst system; B) polymerization is carried out using the catalyst system by bringing it into contact with at least a C ₃ -C ₁₂ - α -olefin, whereupon poly-C ₃ -C ₁₂ - α -olefin chains are formed in the catalytically active titanium groups, and preferably by bringing the said catalyst system, the said C ₃ -C ₁₂ - α -olefin and the said poly-C ₃ -C ₁₂ - α -olefin chains into contact with hydrogen or some other similar chain transfer agent, whereupon a poly-C ₃ -C ₁₂ - α -olefin terminated with hydrogen or suchlike is formed. In the process the improvement is achieved so that, in step A), i) a first controlled amount of a less soluble internal donor and a second controlled amount of a more soluble internal donor are provided on the surface of the said support, titanated support or activated support, in order to produce an internal donation product, and ii) the internal donation product is brought into contact with at least one eluant eluting the more soluble internal donor and with at least one external donor or a reagent forming it, in order to produce an external donation product, the catalyst system thereby formed having at least catalytically active titanium groups, the said first controlled amount of the less soluble internal donor and the said second controlled amount comprising external donor.			

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Process for the polymerization of α -olefins, a catalyst used in the polymerization and its preparation

The invention relates to a process for the polymerization of C_3 - C_{12} - α -olefins, wherein

A) a catalyst system is prepared by bringing a support which comprises magnesium chloride, a derivative thereof or a reagent forming it into contact with at least titanium tetrachloride or a reagent forming it, in order to produce a titanated support, by bringing the titanated support into contact with at least a compound of a metal of group 1, 2 or 13 of the Periodic Table of the Elements (IUPAC 1990), which compound contains a C_1 - C_{10} -alkyl and activates titanium tetrachloride to a catalytically active titanium group, in order to produce an activated support, and by bringing a substance selected from among the said support, titanated support and activated support into contact with at least one donor or a reagent forming it, in order to produce a catalyst system;

B) polymerization is carried out by using the catalyst system by contacting it with at least a C_3 - C_{12} - α -olefin, whereupon poly- C_3 - C_{12} - α -olefin chains are formed in the catalytically active titanium groups, and preferably by contacting the said catalyst system, the said C_3 - C_{12} - α -olefin and the said poly- C_3 - C_{12} - α -olefin chains with hydrogen or some other similar chain transfer agent, whereby a poly- C_3 - C_{12} - α -olefin terminated with hydrogen or suchlike is formed.

The invention also relates to a method for the preparation of a catalyst system intended for the polymerization of C_3 - C_{12} - α -olefins, in which process a support which comprises magnesium chloride, a derivative thereof or a reagent forming it is contacted with at least titanium tetrachloride or a reagent forming it, in order to form a titanated support; the titanated

support is contacted with at least a compound of the said group 1, 2, or 13 metal, which compound contains a C_1 - C_{10} -alkyl and activates titanium tetrachloride to a catalytically active titanium group, in order to produce an activated support; and a substance selected from among the said support, titanated support and activated support is contacted with at least one donor or a reagent forming it, whereby the said catalyst system is formed.

By titanated support is meant a contact product of a support and titanium tetrachloride or a reagent forming it. By activated support is meant a support which has first been contacted with titanium tetrachloride or a reagent forming it, and thereafter with a metal compound which contains a C_1 - C_{10} -alkyl and activates titanium tetrachloride.

Finally the invention relates to a catalyst system intended for the polymerization of C_3 - C_{12} - α -olefins, the catalyst system being prepared by the above method for the preparation of a catalyst system.

The conventional process for the polymerization of poly- C_3 - C_{12} - α -olefins has the disadvantage that all of the donors used therein participate in a random equilibrium system. Thus the quantity and quality of the poly- C_3 - C_{12} - α -olefin fractions depending on equilibrium cannot be regulated. This has resulted, for example, in that, when the isotacticity of the product is raised by using a larger donor quantity, the hydrogen sensitivity of the catalyst system has decreased and its activity has dropped.

In the said step A) of the polymerization process, when a support comprising magnesium chloride, a derivative thereof or a reagent forming is contacted with titanium tetrachloride or a reagent forming it, there is formed a titanated support having at least titanium tetrachloride coordinated to its magnesium

chloride.

Thus, when the said titanated support is contacted with a metal compound containing a C_1 - C_{10} -alkyl, there is formed an activated support having catalytically active titanium groups coordinated to its magnesium chloride.

Finally, when a substance selected from among the said support, titanated support and activated support is contacted with at least one donor or a reagent forming it, a catalyst system is formed the activated support of which has, coordinated in its magnesium chloride, catalytically active titanium groups and at least one type of donor.

An object of the present invention is to provide a poly- C_3 - C_{12} - α -olefin as isotactic as possible, without reducing the hydrogen sensitivity or activity of the catalyst system.

The above-mentioned objects of the invention have now been achieved by a novel process for the polymerization of C_3 - C_{12} - α -olefins, the process being primarily characterized in that in step A):

- i) on the surface of the said support, titanated support or activated support there is provided a first controlled amount of a less soluble internal donor and a second controlled amount of a more soluble internal donor to produce an internal donoration product, and
- ii) the internal donoration product is contacted with at least one eluant eluting the more soluble internal donor and with at least one external donor or a reagent forming it, in order to produce an external donoration product,

the catalyst system thereby formed containing at least catalytically active titanium groups, the said first controlled amount

of the less soluble internal donor, and the said second controlled amount comprising the external donor.

According to one embodiment, two eluants are used.

In this case, the internal donoration product is contacted with a first eluant, which primarily removes only the coordinated more soluble internal donor, in order to produce a first elution product, which contains, on the surface of the support, treated support, or further treated support, at least the said controlled amount of the less soluble internal donor. Thereafter the first elution product is contacted with at least the external donor or the reagent forming it, in order to produce an external donoration product, which contains, on the surface of the support, treated support, or further treated support, at least the said controlled amount of the less soluble internal donor and external donor, i.e. the external donor has replaced the more soluble internal donor.

Finally the external donoration product is contacted with a second eluant, which removes external donor from the surface of a support of the type concerned and yields external donor back to the surface concerned, in order to produce a second elution product, which contains, on the surface of the support, treated support or further treated support, at least the said controlled amount of the less soluble internal donor and additionally external donor in a thermodynamic equilibrium.

In the obtained catalyst system, on the surface of the support of the external donoration product or optionally the second elution product there is thus, coordinated, at least catalytically active titanium groups, the said controlled amount of the less soluble internal donor and external donor in equilibrium, the second eluant maintaining the said equilibrium.

Although it is possible in the invention to elute in step ii)

substantially all of the more soluble internal donor from the surface of the support concerned, according to one embodiment it is also possible in step ii) to use such an amount or type of eluant that it removes only a portion of the more soluble internal donor, in which case the catalyst system obtained contains, coordinated, a catalytically active titanium group and, in a controlled ratio, less soluble internal donor, more soluble internal donor, and external donor.

The present invention is thus based on the realization that, instead of one internal donor or a reagent forming it, two internal donors or reagents forming them are used, one of the donors being a less soluble internal donor or a reagent forming it and the other a more soluble internal donor or a reagent forming it. By contacting a substance selected from among a support, a titanated support and an activated support with the less soluble internal donor or a reagent forming it and with the more soluble donor or a reagent forming it, in a controlled ratio, and by replacing the more soluble internal donor with the external donor, the ratio desired in the given case is always obtained between the internal donor and the external donor.

As it has been observed in the invention that the different fractions of poly-C₃-C₁₂- α -olefins are adjustable and that an isotactic material can be prepared with a greater hydrogen sensitivity and a greater yield than previously, in its widest scope the invention relates only to the procedures stated in the foregoing and hereinafter.

Typical C₃-C₁₂- α -olefins usable in the polymerization process according to the invention include propylene, 1-butene, 4-methyl-1-pentene, 3-methyl-1-butene, 4,4-dimethyl-1-pentene, etc. They may also be copolymerized with one another and with other monomers, preferably ethylene. The most preferred C₃-C₁₂- α -olefin is propylene.

According to a preferred embodiment of the invention, in polymerization step B) the said catalyst system, the said C_3 - C_{12} - α -olefin and the said poly- C_3 - C_{12} - α -olefin chains are contacted with hydrogen or other such chain transfer agent, whereupon a hydrogen-terminated poly- C_3 - C_{12} - α -olefin is formed.

In the polymerization process according to one embodiment of the invention, there are two internal donor types, of which the first is poorly soluble in trialkylaluminum and the second is more soluble in trialkylaluminum, which acts both as the activating C_1 - C_{10} -alkyl metal compound and as an eluant. Thus the polymerization system is controlled and the amount of internal donor eluted by alkylaluminum is no longer random but controlled. It is to be noted in this context that the above systems also enable eluants other than trialkylaluminum to be used, a fact which in turn increases the controllability of the polymerization process. An embodiment in which at least two eluants are used has also been described above. The invention thus relates to a control method by which various desired poly- α -olefin products are achieved and not to a certain set of parameter values by the use of which only a specific poly- α -olefin product is arrived at.

Donors or reagents forming them do not compete with titanium tetrachloride or a reagent forming it for the coordination sites of magnesium chloride or a derivative thereof. Furthermore, since according to the invention it is possible to use an eluant which is not necessarily a metal compound which contains a C_1 - C_{10} -alkyl and activates titanium tetrachloride, the donation and elution steps according to the invention, described above, can be carried out completely independently of the titanation and activation. Thus, in principle the donation/-elution can be carried out on a support, a titanated support, or an activated support. Also, there is no obstacle to carrying out or continuing the donation and elution also in the said

polymerization step B).

According to one preferred embodiment of the invention, the titanation and activation of step A) are combined with one or more donoration and elution runs of steps i) and ii) according to the invention in such a manner that in step A)

i') a support which comprises magnesium chloride, a derivative thereof or a reagent forming it is contacted with at least titanium tetrachloride or a reagent forming it, with a first separate amount of a less soluble internal donor or a reagent forming it, and with a second separate amount of a more soluble internal donor or a reagent forming it, in order to produce an internally donored and titanated support containing the said first controlled amount of the less soluble internal donor and the said second controlled amount of the more soluble internal donor. In this case the magnesium chloride of the support contains at least coordinated titanium tetrachloride and the above-mentioned less soluble internal donor and more soluble internal donor. Thereafter

ii') the internally donored and titanated support is contacted with at least a compound of a group 1, 2 or 13 metal, which compound contains a C₁-C₁₀-alkyl and activates titanium tetrachloride to a catalytically active titanium group; with at least one eluant, which may be a compound of the said metal, and with at least one external donor or a reagent forming it, in order to produce a catalyst system which contains at least catalytically active titanium groups and, in a controlled ratio, the less soluble internal donor and the external donor.

By the terms presented above, "a first separate amount of a less soluble internal donor or a reagent forming it" and "a second separate amount of a more soluble internal donor or a reagent forming it" is meant the use of two different internal donors or two different reagents forming internal donors, as a

mixture or separately, or the use of the same substance separately as a reagent forming one internal donor (cf. hereinafter transesterification) and as a second internal donor. By "amount" is meant in this context the added amount, not the amount associated with the support.

According to one embodiment, the more soluble internal donor is removed and possibly equilibrated by means of one eluant and the external donor is equilibrated by means of another eluant, in which case in the above-mentioned step ii') the internally donorated and titanated support is contacted with at least a compound of a metal of group 1, 2 or 13, which compound contains a C_1 - C_{10} -alkyl and activates titanium tetrachloride to a catalytically active titanium group, and with a first eluant, which primarily removes only the more soluble internal donor, in order to produce an internally donorated, eluted and activated support having catalytically active titanium groups and a poorly soluble internal donor, as well as uncoordinated coordinative sites left by the removed more soluble internal donor. Thereafter the said internally donorated, eluted and activated support is contacted with at least an external donor or a reagent forming it, which is capable of coordinating to the said coordinative sites, and with a second eluant, which removes external donor from the said coordinative sites and yields it back, in order to produce a catalyst system which has, in the magnesium chloride of its twice donorated and eluted and activated support, at least coordinated catalytically activated titanium groups and, in a controlled ratio, the less soluble internal donor and the external donor in equilibrium, the said second eluant maintaining the equilibrium.

When in step B) the said catalyst system is contacted with a C_3 - C_{12} - α -olefin, there form, in the catalytically active titanium groups adjacent to the coordinated less soluble internal donor, long, completely isotactic poly- C_3 - C_{12} - α -olefin chains and, in the catalytically active titanium groups ad-

jacent to the coordinated external donor and the coordinative sites in equilibrium with it, there form isotactic chain sequences of poly-C₃-C₁₂- α -olefins or short atactic chains or chain sequences, depending on whether the external donor is respectively linked to the coordinative sites or separate therefrom.

When in step B) the said catalyst system, the said C₃-C₁₂- α -olefin and said poly-C₃-C₁₂- α -olefin chains are contacted with hydrogen or other such chain transfer agent, there occurs linking of a first atom of hydrogen to the catalytically active titanium groups adjacent to the coordinative sites and of a second atom of hydrogen to the atactic poly-C₃-C₁₂- α -olefin chains and sequences in the said groups, whereby hydrogen-terminated poly-C₃-C₁₂- α -olefin is formed.

By the use of at least two internal donors of clearly different solubilities it is thus possible better to control the polymerization process according to the invention. According to one embodiment, the proportion of purely isotactic and larger-molecule material in the poly-C₃-C₁₂- α -olefin containing it and a less isotactic and smaller-molecule material is controlled by means of the ratio of the less soluble internal donor to the more soluble internal donor so that with larger proportions of less soluble internal donor a larger proportion of purely isotactic and larger-molecule material is obtained. Respectively, with smaller proportions of less soluble internal donor a smaller proportion of purely isotactic and larger-molecule material is obtained.

Depending on whether or not, during the polymerization, the external donor participating in the equilibrium is attached to the support, alternating isotactic and atactic sequences are formed. Since chain transfer by means of hydrogen occurs only at the stage of growth of atactic sequences, isotactic sequences are in general longer than atactic sequences. According

to one embodiment of the invention, the proportion of isotactic material in the form of chain sequences in the less isotactic and smaller-molecule (thus not purely isotactic) material of poly-C₃-C₁₂- α -olefin is controlled by means of the ratio of the external donor to the second eluant so that with a larger amount of external donor in proportion to the second eluant a larger proportion of an isotactic and larger-molecule material in the form of sequences is obtained. Thus there forms a material which is isotactic but at the same time more hydrogen-sensitive than when a large amount of the less soluble internal donor is used. Respectively, when less eluant and more external donor is used, a larger proportion of atactic and smaller-molecule material in the form of sequences is obtained. Thus there also forms a larger amount of the said xylene-soluble, completely atactic material having a very small molecular size.

Above, the control of the different fractions of poly-C₃-C₁₂- α -olefins by means of donors and eluants, in accordance with the invention, has been described. The said fractions can also be affected by means of other parameters, such as the reaction time, the reaction temperature and the amount of the chain transfer agent, such as hydrogen. It is thus preferable to adjust the length and molecular weight of the chain sequences and/or chains of the less isotactic and smaller-molecule material of the poly-C₃-C₁₂- α -olefin by means of hydrogen and/or the temperature so that with a lower hydrogen amount and a lower temperature a higher molecular weight is obtained, and vice versa. The molecular weight is in general measured by using the melt index, MFR, a lower MFR being obtained with higher molecular weights.

A wide molecular weight distribution can be achieved by using, for example, approximately equal amounts of the less soluble internal donor and the external donor, the latter splitting off in a state of equilibrium, whereupon approximately equal amounts of a larger-molecule isotactic material and a smaller-

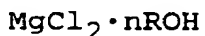
molecule atactic material are formed. Furthermore, the molecular weight of the atactic material can be decreased further by using a large amount of hydrogen. By the control method according to the invention, poly- α -olefins suitable for different uses can thus be obtained.

~~In steps i) and i')~~ stated above, the said less soluble internal donor is preferably a Lewis base less soluble in a hydrocarbon. Internal donors are well known in the art, and lists thereof have been presented widely in the patent literature and in scientific literature. Thus a person skilled in the art will know what is meant by an internal donor. The internal donor is thus a Lewis base, which means that its molecule has one or more electron-donor heteroatoms, such as oxygen, nitrogen, phosphorus or sulfur atoms. In general, bidentate (= two electron-donor heteroatoms) Lewis bases are used in the polymerization of poly-C₃-C₁₂- α -olefins, and thus it is advantageous to use a bidentate Lewis base poorly soluble in a hydrocarbon. Respectively, the more soluble internal donor is preferably a Lewis base more soluble in a hydrocarbon, most preferably a bidentate Lewis base more soluble in a hydrocarbon. By "less soluble" and "more soluble" are meant within the widest scope of the invention materials that are less soluble or more soluble than the other in the eluant used. It is clear that, when an eluant is added according to the invention, the purpose is in general to remove the more soluble internal donor but to leave as much as possible (preferably all) of the less soluble internal donor in the solid catalyst.

According to one preferred embodiment, the less soluble internal donor is a C₁-C₆-alkyl ester of an organic carboxylic acid, preferably a C₁-C₄-alkyl ester of an organic dicarboxylic acid, and most preferably diethyl phthalate. It is known that a low-alkyl diethyl phthalate attached to a solid catalyst is very difficult to elute. This may be due to the fact that the small alkyl groups, i.e. ethyls, of phthalate are not solvated as

strongly with a hydrocarbon solvent or a hydrocarbon-containing solvent, i.e. the eluant, as are the larger alkyls of a phthalate. When phthalates are used, the preferred difference in the alkyls between the less soluble and the more soluble internal donors is at least 3, preferably at least 6, carbon atoms.

Since it is difficult to attach di-C₁-C₄-alkyl phthalate, preferably diethyl phthalate, directly to a support, a titanated support or an activated support, it can advantageously be formed by using as the magnesium chloride derivative in step i) or i') a complex according to Formula I:



(I)

where ROH is an aliphatic C₁-C₄-alcohol, preferably ethanol, or a mixture of such alcohols, n is 1-6, preferably approx. 3. A di-C₇-C₂₀-alkyl phthalate, preferably dioctyl phthalate, is used as the reagent forming the less soluble internal donor. Thereafter they are transesterified to a di-C₁-C₄-phthalate, preferably diethyl phthalate, coordinated to magnesium chloride, and to a removable C₇-C₂₀-alcohol byproduct, preferably octanol. Transesterification can be effected not only by the above-mentioned reagent selection but also by using a high temperature, i.e. a temperature of approx. 128-200 °C, preferably approx. 130-150 °C.

According to one preferred embodiment, the more soluble, i.e. elutable, internal donor of step i) and i') is a C₇-C₂₀-alkyl ester of an organic carboxylic acid, preferably a di-C₈-C₁₆-alkyl ester of organic dicarboxylic acid, such as dioctyl phthalate, dinonyl phthalate, didecyl phthalate, diundecyl phthalate, didodecyl phthalate, ditridecyl phthalate or ditetradecyl phthalate. The most preferable phthalate is dioctyl phthalate. Since the low solubility of the less soluble internal donor was probably due to the short alkyl group of the

phthalate, the higher solubility of the more soluble internal donor is most likely respectively due to the greater length of the alkyl group of the phthalate, enabling the donor to be solvated by a hydrocarbon and be removed.

Since the substance forming the less soluble internal donor may ~~be the more soluble internal donor, the first-mentioned internal~~ donor can advantageously be prepared by partial transesterification. In this case the said controlled amounts of the less soluble and more soluble internal donor are obtained by carrying out the said transesterification in a limited manner, in which case the unreacted amount of di-C₇-C₂₀-alkyl phthalate constitutes the said amount of the more soluble donor. Preferably the limited transesterification is carried out by adjusting the ratio of the complex to di-C₇-C₂₀-alkyl phthalate, the reaction temperature and/or the pressure.

It is preferable to use in step i) and i') a molar ratio of the less soluble + the more soluble internal donor to magnesium which is within a range of 0.10-0.50, preferably 0.10-0.40, and most preferably 0.15-0.30.

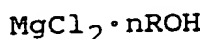
As was pointed out above, the one or more eluants in step ii) and ii') may either be a separate eluant or be of the same metal compound which contains C₁-C₁₀-alkyl and activates coordinated titanium tetrachloride to a catalytically active titanium group. The eluant is thus an organic substance which dissolves the more soluble internal donor but does not dissolve the less soluble internal donor. Thus the more soluble internal donor and the less soluble internal donor together with the eluant form a dissolution system which elutes out most or all of the more soluble internal donor but leaves most of the less soluble internal donor in the support, the titanated support or the activated support. By organic material is meant in this context both purely organic and organometallic materials.

According to one preferred embodiment, the eluant is a group 1, 2 or 13 metal compound which contains a C₁-C₁₀-alkyl, preferably such an excess of the metal compound containing a C₁-C₁₀-alkyl, and being used in step A) for activation purposes, that it does not participate in the activation of the coordinated titanium tetrachloride to a catalytically active titanium group. A preferred eluant is tri-C₁-C₁₀-alkylaluminum, a more preferable eluant is tri-C₁-C₆-alkylaluminum, and the most preferred is tri-C₁-C₄-alkylaluminum, such as triethylaluminum. The molar ratio Al/Ti is preferably within a range of 1-2000, preferably within a range of 50-500, and most preferably within a range of 100-200.

In steps ii) and ii') a treatment with an external donor and an eluant is carried out. The said external donor is according to a preferred embodiment a Lewis base partly soluble in hydrocarbon, and preferably a bidentate Lewis base partly soluble in hydrocarbon. By "partly soluble" is meant that the external donor is partly attached to a solid catalyst and partly, eluted by the said eluant, in solution, i.e. the external donor, together with the catalyst and the eluant, forms an equilibrium system. The external donor is a typical external donor used in the art. Lists of external donors can be found in the literature of the field, and a person skilled in the art will be capable of selecting from them suitable external donors the solubility of which corresponds to the criteria stated above. A typical external donor is a dialkyl-dialkoxysilane, such as cyclohexyl-methyl-dimethoxysilane.

As was pointed out, in the process according to the invention for the polymerization of C₃-C₁₂- α -olefins, such as propylene, a support is used which comprises magnesium chloride, a derivative thereof or a reagent forming it. The support itself may be magnesium chloride, a derivative thereof or a reagent forming it, or the support may be, for example, of an inert substance, such as an inorganic oxide, coated with magnesium chloride, a

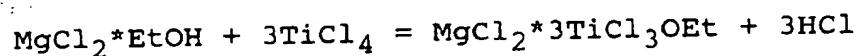
derivative thereof or a reagent forming it. Some typical inert supports are silica, alumina, their mixtures or mixed oxides with each other or with other oxides. A preferred magnesium chloride is β -magnesium chloride, which coordinates titanium tetrachloride well. β -magnesium chloride is formed, for example, by grinding or through chemical reactions. Examples of derivatives of magnesium chloride include its complexes with alcohols and examples of reagents forming magnesium chloride include alkyl magnesium compounds and magnesium alkoxy compounds, which together with a chlorinating substance form β -magnesium chloride. According to a preferred embodiment, the magnesium chloride derivative comprised by the support is a complex according to generic Formula (I)



(I)

where ROH is an aliphatic C_1 - C_4 alcohol or a mixture of such alcohols, and n is 1-6, preferably approx. 3, in which case in step A) this complex is caused to react with titanium tetrachloride or a complex forming it. R is preferably methanol and/or ethanol, most preferably ethanol.

A typical reaction in which a reagent according to Formula (I) reacts with titanium tetrachloride occurs according to the following reaction equation:

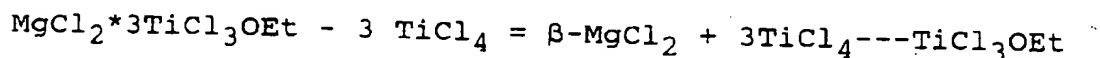


where Et is the ethyl group C_2H_5 . It should be pointed out that the alcohol, which is sometimes called an electron donor in the literature, is not an internal electron donor, since it leaves the catalyst system during titaniation. The same, of course, concerns all compounds reacting in this manner.

In this reaction, three moles of TiCl_3OEt are formed for each mole of MgCl_2 . The TiCl_3OEt formed must be removed by washing

as completely as possible, since this byproduct is a catalyst poison in the polymerization of propylene or any other C_3 - C_{12} - α -olefin. Therefore the reaction is performed in the presence of a large $TiCl_4$ excess, the hot $TiCl_4$ washing out the $TiCl_3OEt$ byproduct. According to a preferred embodiment, titanium tetrachloride or a reagent forming it is used in such an excess that the molar ratio $Ti/Mg = 1-100$, preferably $5-40$, most preferably $10-25$.

In the titanium chloride wash, magnesium chloride in its coordinative form, i.e. β -form, is released according to the following reaction equation:



A portion of the titanium tetrachloride coordinates to β - $MgCl_2$ and forms active centers during activation. To make the titanium tetrachloride wash more effective, preferably at least two, and most preferably three, titanium tetrachloride treatments are used.

By the reagent which forms titanium tetrachloride used in the titanation is meant, for example, titanium alkoxide or titanium alkoxychloride, which together with a chlorination reagent form titanium tetrachloride which can be activated.

According to a preferred embodiment of the invention, in step A) at least three steps are performed, in the first of which the support is contacted with titanium tetrachloride or a reagent forming it and with the less soluble internal donor or a reagent forming it; in the second the solid obtained from the first step is contacted with titanium tetrachloride or a reagent forming it and with the more soluble internal donor or a reagent forming it; and in the third the solid obtained from the second step is contacted with titanium tetrachloride or a corresponding washing solvent.

Most preferably, in the first step a complex of magnesium chloride and alcohol (cf. Formula (I) above) is used as the magnesium chloride derivative and di-C₇-C₂₀-alkyl phthalate as the reagent forming the less soluble internal donor, and the conditions used are such that, in the first step, there occurs forming and linking in situ of the less soluble internal donor (cf. transesterification above), in which case, in the second step, the second, more soluble internal donor is linked to the solid catalyst intermediate by normal coordination. Preferably the said steps are combined, i.e. a partial transesterification to a less soluble C₁-C₄-alkyl ester and a more soluble C₇-C₂₀-alkyl ester is carried out.

In step A) of the process according to the invention, the preferable molar ratio of the less soluble internal donor to magnesium is within a range of 0.05-0.30, most preferably within a range of 0.10-0.20. When step A) is carried out in three steps, it is preferable to use in the first step a molar ratio of the less soluble internal donor to magnesium which is within a range of 0.05-0.30, preferably within a range of 0.10-0.20. Respectively, it is advantageous to use in general, and preferably in the said second step, a molar ratio of the more soluble internal donor to magnesium which is within a range of 0.05-0.30, most preferably within a range of 0.10-0.20. Most preferably, substantially equal amounts of the less soluble and of the more soluble internal donor are used, i.e. the molar ratio of the less soluble internal donor to the more soluble internal donor is preferably within a range of 0.5-2.0, more preferably within a range of 0.7-1.3, and most preferably approx. 1.0.

In the step in which the coordinated titanium tetrachloride is activated by means of a group 1, 2 or 13 metal compound containing a C₁-C₁₀-alkyl it is preferable to use a compound which reduces and C₁-C₁₀-alkylates the coordinated titanium tetrachloride to a catalytically active titanium group. Thereby the

titanium tetrachloride is reduced and the C₁-C₁₀-alkyl group of the said metal compound links to it; during the polymerization, C₃-C₁₂- α -olefin monomers are linked to the C₁-C₁₀-alkyl group.

These compounds, defined as cocatalysts, which are capable of reducing and alkylating titanium tetrachloride to a catalytically active titanium group, are well known in the art. A typical metal compound which contains C₁-C₁₀-alkyl is a tri-C₁-C₁₀-alkylaluminum, preferably a tri-C₁-C₆-alkylaluminum, and most preferably a tri-C₁-C₄-alkylaluminum, such a triethylaluminum. When reagents to be chlorinated, forming magnesium chloride and/or titanium chloride, are used, it is possible to use C₁-C₁₀-alkylaluminum chlorides, which both activate and chlorinate the said reagents. A preferred Al/Ti molar ratio is 1-2000, more preferable 50-500, and the most preferable 100-200.

As was mentioned at the beginning, the invention relates not only to the polymerization process described above but also to a method for the preparation of the catalyst system used in the polymerization and to the said catalyst system. The catalyst system according to the invention and its preparation are evident from the polymerization process described above, if steps A), i), i'), ii), and ii') of the polymerization process are taken into account. In this context we also refer to accompanying Claims 24 and 25.

Experiments, in which 21 examples were performed, are described below. The description is of the empirical progress towards the invention, and thus Examples 1-4, A and J are reference examples, whereas Examples 5, 6 and B-O describe the present invention, using two internal donors D₁.

Examples

In the research, larger donor amounts in one and the same titration step (cf. for example 1 and 2) and different donor

amounts in two successive titanation steps were used. The investigation thus related not only to the effect of increasing donor amounts in one and the same titanation step but also to their division among different titanation steps.

In Reference Examples 1 and 2 of the preliminary experiment series, an investigation was made whether it was possible to use larger donor amounts together with transesterification to raise the isotacticity index II without a decrease in the hydrogen sensitivity (MFR) or the activity of the catalysts. In these experiments, two normal titanation runs were performed, an internal donor being added to the first of them and the second one being carried out as a washing step without a donor. The ratio of internal donor D_1 to magnesium Mg used was $D_1/Mg = 0.15$ and 0.3 (Examples 1 and 2).

In Reference Example 3 of the preliminary experiment series, three titanation steps were experimented with; only to the first of them was one type of internal donor added to investigate whether it was possible to wash off the detrimental byproducts of catalyst preparation without the isotacticity index II decreasing owing to the repeated titanium tetrachloride washes.

In Reference Example 4, the increasing of the donor amount in comparison to Example 3 in the first titanation step of the titanation was experimented with in order to determine whether such a procedure would provide any advantages with respect to the isotacticity - hydrogen sensitivity - activity equilibrium. In this example, a D_1/Mg ratio of 0.3 was used.

In Embodiment Example 5, two internal donors were added in different steps, in the first titanation step and in the second titanation step, whereas the third titanation step, i.e. rinsing titanation, was carried out using titanium tetrachloride without an addition of internal donor. The idea of two internal

donors according to the invention was thus implemented in these examples. The adding of the less soluble internal donor in the first step was carried out by transesterifying the alcohol of $\text{MgCl}_2 \cdot n\text{ROH}$ and an added substance forming the first internal donor, this substance being dioctyl phthalate (DOP), whereby diethyl phthalate (DEP) was obtained, which adhered strongly to the catalyst. The more soluble internal donor (DOP) was added in connection with the second titanation step, without transesterification, whereupon the DOP could be eluted out. In this manner, the system of two donors according to the invention is formed, of which donors one is easily eluted and the other is closely linked to a solid catalyst component, in which case there are better possibilities for controlling the hydrogen sensitivity of the catalyst and the isotacticity, molecular weight and molecular weight distribution of the polymer.

In Embodiment Example 6, the more soluble internal donor used was a compound having a larger hydrocarbon group (in the case of esters, the alkyl group of the alcohol residue). In this example, the aim was also to determine whether these larger molecules could be used in the second donor addition to produce a more soluble activation byproduct $\text{TiCl}_3\text{-OR}$. Thus, in Example 2, dioctyl phthalate (DOP) was used as the reagent forming the less soluble internal donor (DEP) and diundecyl phthalate (DUP) was used as the more soluble internal donor.

Preparation of procatalyst

Unless otherwise mentioned, the procatalyst was prepared according to the following recipe:

45 g of $\text{MgCl}_2 \cdot 3\text{EtOH}$ support was introduced into the synthesis reactor together with 150 ml of heptane. The slurry was cooled to $-10\text{ }^\circ\text{C}$ (stirrer speed was 200 rpm). 300 ml of cold ($-12\text{ }^\circ\text{C}$) titanium tetrachloride TiCl_4 was added into the reactor. The molar ratio $\text{TiCl}_4/\text{EtOH}$ was 4.8. The temperature was raised

within 3 hours to 20 °C. Thereafter a compound forming the internal donor was added, the compound being dioctyl phthalate (DOP). The amount of dioctyl phthalate added during the first titanation is shown in Table 1. The temperature of the mixture was thereafter raised to 130 °C. After 1.5 hours the liquid was removed and the temperature was lowered to 120 °C. After an addition of fresh titanium tetrachloride (TiCl_4) (300 ml), the temperature was maintained at 120 °C for one hour. In Examples 7-10 the second internal donor was added after the said second titanium tetrachloride amount had been added. In Examples 4-10 a third titanium tetrachloride treatment was carried out after the said second titanium tetrachloride treatment. Finally the catalyst was washed 3 times with 300 ml of hot heptane (>90 °C) and was dried by blowing nitrogen through the catalyst bed until the catalyst turned into a freely flowing powder.

Bulk homopolymerization of propylene

Propylene was polymerized in a stirred tank reactor having a volume of 5 liters. 0.6 ml of triethylaluminum cocatalyst (TEA), approx. 0.2 ml of a 25 wt.% n-heptane solution of cyclohexyl-methyl-dimethoxysilane (external donor), and 30 ml of n-heptane were mixed together and were reacted for 5 minutes. One-half of the mixture was fed into the polymerization reactor and the other half was mixed with approx. 20 mg of the above-mentioned procatalyst. After another 5 minutes the procatalyst/TEA/external donor/n-heptane mixture was fed into the polymerization reactor. The Al/Ti molar ratio was 500 and the ratio Al/external donor was 20 mol/mol. 70 mmol of hydrogen and 1400 g of propylene were fed into the reactor, and the temperature was raised within 15-30 minutes to the desired polymerization temperature of 70 °C. The polymerization time was 60 min, whereafter the formed polymer was withdrawn from the reactor. The isotacticity index II and melt index MFR_2 (g/10 min, with a load of 2.16 kg) of the polymer were determined.

Results

Below is a description of the six laboratory catalyst synthesis experiments describing the synthesis differences when a shift is made from two to three titanations, from 0.15 to 0.30 D_1/Mg addition, and from one to two donor additions.

Table 1

Results of bulk homopolymerization of propylene when 2 or 3 titanations (titanium tetrachloride treatments), $D_1/Mg = 0.15$ and 0.3, and the addition of 1 or 2 donors are used.

Quantity	Ref. Ex. 1	Ref. Ex. 2	Ref. Ex. 3	Ref. Ex. 4	Ex. 5	Ex. 6
Titanation times	2	2	3	3	3	3
Donor	DOP	DOP	DOP	DOP	2*DOP	DOP+DUP
D_1 , D_1/Mg , mol/mol	0.15	0.3	0.15	0.3	0.15+0.15	0.15+0.15
Activity kg/g cat.	24.1	24.6	44.9	34.3	38.5	45.3
II %	96.8	98.3	96.2	98.0	97.3	98.2
MFR ₂ , g/10 min	6.4	4.4	7.3	4.7	7.3	8.2

Examination of the results

Reference Example 1. In this example, which represents the classical synthesis, two titanation runs and a D_1/Mg ratio of 0.15 are used. Owing to the low washing efficiency, the activity is only of the order of 25 kg PP/g cat, and owing to the low donor concentration, the isotacticity index II % is lower than 97 %. (It can be assumed that the slightly higher MFR is due to the corresponding isotacticity.)

Reference Example 2. When an attempt is made to correct the

situation in Example 1 with respect to isotacticity by raising the donor amount to 0.3, isotacticity rises to a good value of 98.3, but at the same time hydrogen sensitivity decreases (molecular weight is not decreased, i.e. MFR does not rise), since a larger amount of well-attaching DEP takes up donor sites in the catalyst, and only a lower number of active sites ~~are involved in the hydrogen-sensitive equilibrium of the external donor~~. This is seen as a low melt index (MFR = 4.4). The large amount of DEP also has the effect that activity remains low.

Reference Example 3. When a third titaniation is added to the synthesis, the washing efficiency increases. Owing to the improved washing efficiency, the byproduct, TiCl_3OEt , of the procatalyst is washed out more effectively, and thus the poison effect of this byproduct on the catalyst is reduced. This is seen as a considerable increase in activity ($A = 44.9$). The efficient wash is also seen as a lower donor concentration in the catalyst, which leads to lower isotacticity. The smaller donor amount, for its part, is seen as a higher hydrogen sensitivity, since a larger number of active sites are now involved in the equilibrium of the external donor (MFR = 7.3).

Reference Example 4. If the situation in Example 3 is corrected by adding a larger amount of donor (0.3 DOP), a clearly higher DEP concentration in the catalyst (DEP = 10.9), i.e. a more complete transesterification, is achieved. This leads to a slight decrease in activity as compared with Example 3, owing to the high DEP concentration. The high DEP concentration is also seen as a high isotacticity (98.0 %) and also as a lower melt index. It can be assumed that hydrogen sensitivity decreases as a large amount of internal donor remains attached to the catalyst. The low MFR obtained in the experiment is due to this.

Example 5. In the fifth experiment, it was investigated whether

the donor composition could be changed by adding the DOP donor in two steps. This was possible, since there was still a third titanation available for the washing. The DOP amount added was the same as in Example 4, but it was added in two equal batches, to the first and the second titanation steps. The result showed that the DEP amount obtained by transesterification halved to 4.3, and the amount of DOP obtained by coordination increased to 8.8 %. This corresponded to the expectations. Washing became more effective, since the titanium concentration decreased 1.9 %. The efficient TiCl_3OEt wash and the slight DEP amount increased the activity to 38.5 kg PP/g cat. The DEP + DOP mixture which was obtained by using this synthesis modification proved to be effective in increasing both isotacticity and hydrogen sensitivity, the II % being 97.3 and the MFR being 7.3. The experiment showed that with this combination a sufficient isotacticity is achieved, but additionally the conditions are good for the elution of internal donor during the polymerization, whereupon an equilibrium interaction is achieved between the detaching donor and the free site, thus making hydrogen termination possible.

Example 6. The last experiment was carried out as in Example 5, except that the DOP used in the second donor addition was replaced with DUP. The results of this experiment emphasized what had been achieved in Experiment 5. The Ti % decreased further down to 1.5 %, showing that the washing efficiency provided by this method was advantageous. The DEP amount also decreased to 3.6 %, and the remaining DUP concentration was 6.5 %. Thus the total amount of donor in this catalyst was clearly less. This was seen as a high activity (45.3 kg PP/g cat). The DEP-DUP donor pair additionally provided a very favorable isotacticity protection and made an effective donor equilibrium possible during polymerization, thus producing a high hydrogen sensitivity. Isotacticity increased to 98.2 %, and MFR was 8.2.

Trial run series

After the laboratory-scale experiments 1-6, three full-scale trial run series were also carried out (respectively Examples A-D, F-H and J-O). In the laboratory, three series of catalysts were prepared, in which there was made a gradual shift from a donor addition in the first titanation (titanation I) to a donor addition in the second titanation (titanation II). All of the catalysts were prepared in completely inert conditions. First, 300 ml of TiCl_4 was added to a reactor and was cooled to $-20\text{ }^\circ\text{C}$. 150 ml of heptane and thereafter 25 g of $\text{MgCl}_2 \cdot 3\text{EtOH}$ support were fed into another reactor. This slurry was also cooled to $-20\text{ }^\circ\text{C}$. The first titanation was initiated by bringing both of the above-mentioned cooled liquids together and by allowing them to react with each other.

Thereafter the temperature was raised to $+20\text{ }^\circ\text{C}$ and the first donor addition was done. Thereafter the temperature was raised to $130\text{ }^\circ\text{C}$, at which the first titanation (transesterification) was carried out in 1.5 hours. Thereafter the titanation solution was replaced with 200 ml of fresh TiCl_4 . The second donor addition was done into the new mixture. The second titanation (only coordination) took place at $120\text{ }^\circ\text{C}$ for 0.5 hour.

The third titanation took place in the same manner, with the difference that no donor was added.

After the TiCl_4 treatment, the procatalyst was washed four times with 400 ml of heptane, $90\text{ }^\circ\text{C}$, 15 minutes. The procatalyst was dried in a nitrogen flow. Polymerization was carried out in the same manner as in the preliminary experiment series.

In the first trial series (B-D; A is a reference example), in the first titanation a di-2-ethyl-hexyl phthalate (DOP) donor and transesterification conditions were used. In the second titanation, diundecyl phthalate (DUP) was added in coordinating

conditions. The total donor amount, i.e. the sum of the donor amounts of the first and second additions, was the same in all of the experiments. Calculated in moles, the donor amount was 0.3 in proportion to magnesium, i.e. the donor/Mg molar ratio was 0.3. The DOP, which was added in the first titanation, became transesterified to diethyl phthalate (DEP) owing to the high temperature. The DUP, added in the second titanation, did not become transesterified, since the temperature in the second titanation was lower than in the first titanation. Table 1 shows the donor addition ratios in the first trial series. Table 2 lists the donor compositions of the catalysts after the synthesis, and Table 3 lists the polymer melt indices (MFR₂, g/10 min with a load of 2.16 kg), obtained by test polymerizing the catalysts in question.

Table 1

Donor amounts added in the first trial series

Catalyst	DOP/Mg Titanation I	DUP/Mg Titanation II
Reference example A	0.3	0.0
B	0.25	0.05
C	0.10	0.20
D	0.05	0.25

Table 2

Donor compositions in the catalysts after synthesis

Catalyst	DEP wt. %	DEP mol. %	DUP wt. %	DUP mol. %
Ref. A	10.9	0.049	0	0
B	8.5	0.038	3.0	0.006
C	2.1	0.009	8.0	0.017
D	1.2	0.005	13.6	0.029

Table 3
Melt indices (MFR) of the polymers

Catalyst	MFR
Ref. A	4.7
B	5.0
C	6.7
D	8.0

The results show that a clearly increasing hydrogen sensitivity (MFR) was achieved in the catalysts when a shift was made from only transesterified, well attached internal donor to a donor mixture which also contained a more easily detaching internal donor. In almost all of the catalysts the activity was at a satisfactory level, being around 30 kg/g cat. In the example in which diundecyl phthalate was added to the second titration (not shown in the table), an activity was observed which remained at a lower level. A slight decrease in isotacticity was observed, from 98 % to slightly below 97 %. However, this decrease in isotacticity is not significant in an industrial process.

In the second trial series, DOP was used in both donor additions (transesterification and coordination). Table 4 lists the donor amounts added, Table 5 lists the donor compositions in the catalysts after synthesis, and Table 6 lists the melt indices (MFR) of the polymers.

Table 4

Donor amounts added in the second trial series

Catalyst	DOP/Mg Activation I	DOP/Mg Activation II
Reference example A	0.3	0.0
F	0.2	0.1
G	0.15	0.15
H	0.05	0.25

Table 5

Donor compositions in the catalysts

Catalyst	DEP wt. %	DEP mol. %	DOP wt. %	DOP mol. %
Ref. A	10.9	0.049	1.3	0.003
F	7.5	0.034	6.9	0.018
G	4.3	0.019	8.8	0.023
H	1.1	0.005	10.4	0.027

Table 6

Melt indices (MFR) of the polymers

Catalyst	MFR
Ref. A	4.7
F	4.5
G	7.3
H	6.8

The results show that an increasing hydrogen sensitivity was achieved in the catalyst series when the well-attaching internal donor (DEP) was partly replaced with an easily detached

internal donor (DOP). The isotacticity values in all of the polymers were very good, all being around 98 %. The activities were of the normal level, around 30 kg/g cat. In an example in which DOP was added only to the second titration, a decrease in activity was observed (the example is not shown in the table).

In the third trial series, the first donor addition was maintained constant; the DOP(DEP)/Mg ratio in this addition was 0.15. The donor addition of the second activation was increased gradually from 0.0 up to 0.3. Table 7 lists the donor additions to the synthesis, Table 8 lists the donor compositions of the catalysts after the synthesis, and Table 9 lists the polymer melt indices obtained when the catalysts of this series were test polymerized.

Table 7

Donor additions in the third trial series

Catalyst	DOP/Mg Activation I	DOP/Mg Activation II
J (reference)	0.15	0.0
K	0.15	0.05
L	0.15	0.10
G	0.15	0.15
M	0.15	0.20
N	0.15	0.25
O	0.15	0.30

Table 8

Donor compositions in the catalysts in the third trial series

Catalyst	DEP wt.%	DEP mol.%	DOP wt.%	DOP mol.%
J	5.3	0.024	1.3	0.003
K	5.0	0.023	4.2	0.011
L	4.7	0.021	4.8	0.012
G	4.3	0.019	8.8	0.023
M	3.9	0.018	9.5	0.024
N	5.1	0.023	16.6	0.043
O	3.8	0.017	17.2	0.044

Table 9

Melt indices of the polymers in the third trial series

Catalyst	Melt index (MFR)
J	7.3
K	6.6
L	6.7
G	7.3
M	8.0
N	8.4
O	9.9

The results showed that also in the third trial series an increasing hydrogen sensitivity was achieved in the catalysts, although the change was not as great as in the first two trial series, owing to the constant DOP addition to the first activation. Isotacticity was consistently around 97 % in most of the trial series; only at the extreme points (J, O) was a slightly lower isotacticity (96 %) obtained. The activities remained at

a satisfactory level throughout the trial series, and were all around 30 kg PP/g cat.

The experiments described above show clearly that the catalyst synthesis of two internal donors according to the present invention provides a catalyst system is obtained which yields high isotacticity values while activity and hydrogen sensitivity (\rightarrow lower molecular weight, higher MFR) remain high.

Claims

1. A process for the polymerization of C_3 - C_{12} - α -olefins, wherein

A) a catalyst system is prepared by bringing a support which comprises magnesium chloride, a derivative thereof or a reagent forming it into contact with at least titanium tetrachloride or a reagent forming it, in order to produce a titanated support; by bringing the titanated support into contact with at least a group 1, 2 or 13 metal compound which contains a C_1 - C_{10} -alkyl and activates titanium tetrachloride to a catalytically active titanium group, in order to produce an activated support; and by bringing a substance selected from among the said support, titanated support and activated support into contact with at least one donor or a reagent forming it, in order to produce a catalyst system

B) polymerization is carried out using the catalyst system by bringing it into contact with at least a C_3 - C_{12} - α -olefin, whereupon poly- C_3 - C_{12} - α -olefin chains are formed in the catalytically active titanium groups, and preferably by bringing the said catalyst system, the said C_3 - C_{12} - α -olefin and the said poly- C_3 - C_{12} - α -olefin chains into contact with hydrogen or other similar chain transfer agent, whereupon a poly- C_3 - C_{12} - α -olefin terminated with hydrogen or suchlike is formed,

characterized in that in step a)

i) a first controlled amount of a less soluble internal donor and a second controlled amount of a more soluble internal donor are provided on the surface of the said support, titanated support or activated support, in order to produce an internal donoration product, and

ii) the internal donoration product is brought into contact

with at least one eluant eluting the more soluble internal donor and with at least one external donor or a reagent forming it, in order to produce an external donoration product,

the catalyst system thereby formed having at least catalytically active titanium groups, the said first controlled amount of ~~the less soluble internal donor and the said second controlled~~ amount comprising external donor.

2. A process according to Claim 1, characterized in that in step ii) the internal donoration product is brought into contact with at least one eluant the type and quantity of which only partly remove the more soluble donor, whereupon the catalyst has at least catalytically active titanium groups, the said first controlled amount of the less soluble internal donor and the said second controlled amount which comprises more soluble internal donor and external donor, the said eluant maintaining the equilibrium.

3. A process according to Claim 1 or 2, characterized in that in step A)

i') The support comprising magnesium chloride, a derivative thereof or a reagent forming it is brought into contact with at least:

- titanium tetrachloride or a reagent forming it;
- a first separate amount of the less soluble internal donor or a reagent forming it; and
- a second separate amount of the more soluble internal donor or a reagent forming it, in order to produce an internally donorated and titanated support which has the said first controlled amount of the less soluble internal donor and the said second controlled amount of the more soluble internal donor, and

ii') the internally donorated and titanated support is brought

into contact with at least a group 1, 2 or 13 metal compound which contains a C₁-C₁₀-alkyl and activates titanium tetrachloride to a catalytically active titanium group, with at least one eluant, which may be the group 1, 2 or 13 metal compound which contains said C₁-C₁₀-alkyl, and with at least one external donor or a reagent forming it,

in order to produce a catalyst system which contains at least catalytically active titanium groups, the said first controlled amount of the less soluble internal donor and the said second controlled amount which comprises said external donor.

4. A process according to Claim 1, 2 or 3, characterized in that the proportion of purely isotactic and larger-molecule material in the poly-C₃-C₁₂- α -olefin product of step B) which contains it and a less isotactic and smaller-molecule material is adjusted by means of the ratio of the amount of the less soluble internal donor to the amount of the more soluble internal donor of step i) or i') so that with larger proportions of the less soluble internal donor a larger proportion of purely isotactic and larger-molecule material is obtained, and vice versa.

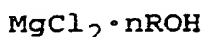
5. A process according to Claim 1, 2, 3 or 4, characterized in that the proportion of the isotactic material in the form of chain sequences in the less isotactic and smaller-molecule material of the poly-C₃-C₁₂- α -olefin product of step B) is adjusted in step ii) or ii') by means of the ratio of the amount of the external donor to the amount of the eluant so that with a larger amount of the external donor in proportion to the eluant a larger proportion of isotactic and larger-molecule material in the form of sequences is obtained, and vice versa.

6. A process according to any of the above claims, characterized in that the length and molecular weight of the chain

sequences and/or chains of the less isotactic and smaller-molecule material of the poly-C₃-C₁₂- α -olefin of step B) is adjusted in step B) by means of hydrogen and/or the temperature so that with a lower amount of hydrogen and a lower temperature a higher molecular weight is obtained, and vice versa.

7. A process according to any of the above claims, characterized in that the said less soluble internal donor of step A) is a C₁-C₆-alkyl ester of an organic carboxylic acid, preferably a C₁-C₄-alkyl ester of an organic dicarboxylic acid, most preferably diethyl phthalate.

8. A process according to Claim 7, characterized in that the less soluble internal donor is a di-C₁-C₄-alkyl phthalate, preferably diethyl phthalate, which is obtained by the transesterification of a magnesium dichloride - alcohol complex according to Formula (I), serving as the magnesium chloride derivative of step A):



(I)

where ROH is a C₁-C₄ alcohol, preferably ethanol, or a mixture of such alcohols, and n is 1-6, preferably approx. 3, and of a di-C₇-C₂₀-alkyl phthalate, preferably dioctyl phthalate, serving as the reagent forming the less soluble internal donor, to a less soluble internal di-C₁-C₄-alkyl phthalate donor, preferably diethyl phthalate, coordinated to magnesium chloride, and a C₇-C₂₀-alcohol, preferably octanol.

9. A process according to any of the above claims, characterized in that the more soluble internal donor of step A) is a C₇-C₂₀-alkyl ester of an organic carboxylic acid, preferably a di-C₈-C₁₆-alkyl ester of an organic dicarboxylic acid, such as dioctyl phthalate, dinonyl phthalate, didecyl phthalate, diundecyl phthalate, didodecyl phthalate, ditridecyl phthalate or ditetradecyl phthalate, most preferably dioctyl phthalate.

10. A process according to Claims 8 and 9, characterized in that the said controlled amounts of the less soluble and the more soluble internal donor are produced by carrying out the said transesterification in a limited manner, in which case the unreacted amount of di-C₇-C₂₀-alkyl phthalate will form the said amount of the more soluble donor.

11. A process according to Claim 10, characterized in that the limited transesterification is carried out by adjusting the ratio of the complex to the di-C₇-C₂₀-alkyl phthalate, the reaction temperature, and/or the pressure.

12. A process according to any of the above claims, characterized in that in step A) the molar ratio of the less soluble plus the more soluble internal donor to magnesium is within a range of 0.10-0.50, preferably within a range of 0.10-0.40, most preferably within a range of 0.15-0.30.

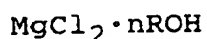
13. A process according to any of the above claims, characterized in that the said at least one eluant of step ii) of step A) is an organic substance which elutes the more soluble internal donor but does not elute the less soluble internal donor, and furthermore, possibly elutes only a proportion of the external donor, preferably a group 1, 2 or 13 metal compound containing C₁-C₁₀ alkyl, more preferably such an excess of the group 1, 2 or 13 metal compound containing a C₁-C₁₀-alkyl, used for the activation of titanium tetrachloride in step A), as does not participate in the activation of the coordinated titanium tetrachloride to a catalytically active titanium group.

14. A process according to Claim 13, characterized in that the eluant is a tri-C₁-C₁₀-alkylaluminum, preferably a tri-C₁-C₆-alkylaluminum, most preferably a tri-C₁-C₆-alkyl aluminum, such as triethylaluminum.

15. A process according to any of the above claims, characterized in that the said external donor is a Lewis base partly soluble in a hydrocarbon, such as a bidentate Lewis base partly soluble in a hydrocarbon, preferably a hydrocarbyl-oxy-silane, most preferably dialkyl-dialkoxysilane, such as cyclohexyl-methyl-dimethoxysilane.

16. A process according to any of the above claims, characterized in that the magnesium chloride comprised by the support of step A) is β -magnesium chloride.

17. A process according to any of Claims 1-15, characterized in that the magnesium chloride derivative comprised by the support of step A) is a magnesium dichloride - alcohol complex according to generic Formula (I):



(I)

where ROH is an aliphatic C_1 - C_4 -alcohol, preferably ethanol, or a mixture of such alcohols, and n is 1-6, preferably approx. 3, this complex being reacted in step A) with at least titanium tetrachloride or a reagent forming it.

18. A process according to Claim 17, characterized in that in step A) an excess of titanium tetrachloride or a reagent forming it is used, preferably in a molar ratio of $\text{Ti/Mg} = 1-100$, more preferably 5-40, most preferably 10-25, in order to rinse off the reaction byproducts of the complex and the titanium tetrachloride or the reagent forming it.

19. A process according to any of the above claims, characterized in that in step A) several, preferably at least three, steps are carried out, in the first of which the support is brought into contact with titanium tetrachloride or a reagent forming it and with the less soluble internal donor or a

reagent forming it, in the second, etc., the solid material obtained from the first step is brought into contact with titanium tetrachloride or a reagent forming it and with the more soluble internal donor or a reagent forming it, and in the third, or the last, the solid material obtained from the second step is brought into contact with titanium tetrachloride or some other washing solvent.

20. A process according to any of the above claims, characterized in that in step A), and preferably in the first step of Claim 19, the molar ratio of the fed-in less soluble internal donor or reagent forming it to magnesium is within a range of 0.05-0.30, preferably within a range of 0.10-0.20.

21. A process according to any of the above claims, characterized in that in step A), and preferably in the above-mentioned second step, the molar ratio of the fed-in more soluble internal donor or reagent forming it to magnesium is within a range of 0.05-0.30, preferably within a range of 0.10-0.20.

22. A process according to any of the above claims, characterized in that the molar ratio of the less soluble to the more soluble internal donor introduced in step i) or i')) is within a range of 0.5-2.0, preferably within a range of 0.7-1.3, most preferably approx. 1.0.

23. A process according to any of the above claims, characterized in that in step A) there is used as the said group 1, 2 or 13 metal compound which contains a C_1 - C_{10} -alkyl a compound which reduces and C_1 - C_{10} -alkylates the titanium tetrachloride present in the magnesium chloride to a catalytically active titanium group, preferably a tri- C_1 - C_{10} -alkylaluminum, more preferably a tri- C_1 - C_6 -alkylaluminum, most preferably a tri- C_1 - C_4 -alkylaluminum such as triethylaluminum.

24. A method for the preparation of a catalyst system intended for the polymerization of C_3 - C_{12} - α -olefins, characterized in that the preparation is carried out by the procedure described in Claims 1-3 and 4-23.

25. A catalyst system intended for the polymerization of C_3 - C_{12} - α -olefins, ~~characterized in that it is prepared by the~~ method according to Claim 24.

INTERNATIONAL SEARCH REPORT

International application No.

PCT/FI 97/00562

A. CLASSIFICATION OF SUBJECT MATTER		
IPC6: C08F 4/654, C08F 10/00 According to International Patent Classification (IPC) or to both national classification and IPC		
B. FIELDS SEARCHED		
Minimum documentation searched (classification system followed by classification symbols)		
IPC6: C08F		
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched		
SE,DK,FI,NO classes as above		
Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)		
CAPLUS, EPODOC		
C. DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	Macromol. Symp., Volume 89, 1995, Norio Kashiwa et al, "Stereoregularity and regioregularity of active centers in propene polymerization", page 27 - page 37, abstract; page 27-28; page 32; page 36	1-25
X	EP 0683175 A2 (MITSUI PETROCHEMICAL INDUSTRIES, LTD.), 22 November 1995 (22.11.95), abstract; claims; page 4, line 40 - page 8, line 2; page 11, line 20 - line 28	1-25
A	EP 0409492 A1 (BP CHEMICALS LIMITED), 23 January 1991 (23.01.91), abstract; claims	1-25
<input checked="" type="checkbox"/> Further documents are listed in the continuation of Box C. <input checked="" type="checkbox"/> See patent family annex.		
* Special categories of cited documents: "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention "X" document of particular relevance: the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone "Y" document of particular relevance: the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art "&" document member of the same patent family		
Date of the actual completion of the international search		Date of mailing of the international search report
11 December 1997		23-12-1997
Name and mailing address of the ISA/ Swedish Patent Office Box 5055, S-102 42 STOCKHOLM Facsimile No. +46 8 666 02 86		Authorized officer Agneta Österman Wallin Telephone No. +46 8 782 25 00

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PCT/FI 97/00562

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Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP 0627449 A1 (NESTE OY), 7 December 1994 (07.12.94), abstract; claims --	1-25
A	EP 489536 A2 (IMPERIAL CHEMICAL INDUSTRIES PLC), 10 June 1992 (10.06.92), abstract, claims -- -----	1-25

INTERNATIONAL SEARCH REPORT

Information on patent family members

04/11/97

International application No.

PCT/FI 97/00562

Patent document cited in search report			Publication date	Patent family member(s)		Publication date
EP	0683175	A2	22/11/95	CA	2149729 A	20/11/95
				CN	1112940 A	06/12/95
				JP	8034813 A	06/02/96
EP	0409492	A1	23/01/91	SE	0409492 T3	
				AT	110394 T	15/09/94
				AU	631910 B	10/12/92
				AU	651006 B	07/07/94
				AU	2624492 A	03/12/92
				AU	6044190 A	22/02/91
				CA	2030515 A	18/01/91
				CN	1049357 A	20/02/91
				DE	69011776 D,T	15/12/94
				ES	2057414 T	16/10/94
				FI	99118 B	30/06/97
				FR	2649708 A,B	18/01/91
				JP	4500832 T	13/02/92
				NO	178863 B,C	11/03/96
				WO	9101338 A	07/02/91
EP	0627449	A1	07/12/94	FI	96615 B,C	15/04/96
				FI	932580 A	05/12/94
				JP	7145205 A	06/06/95
				NO	942056 A	05/12/94
EP	489536	A2	10/06/92	NONE		